Mesoporous TS-1 catalysts were prepared via a nanocasting route using two different carbon template sources of CMK-3 and commercial carbon black. Products were characterized by XRD, UV-Vis spectroscopy, SEM, TEM, and \( \text{N}_2 \) adsorption-desorption measurement. The catalytic performances of the samples for allylchloride epoxidation and oxidative desulfurization of the representative refractory sulfur compounds, dibenzothiophene and 4,6-dimethyl dibenzothiophene, were compared against those of conventional TS-1. Whilst the allylchloride epoxidation activity for the mesoporous TS-1 samples were similar, mesoporous TS-1 exhibited significantly higher catalytic activities than conventional TS-1 in oxidative desulfurization.

**Key Words:** Mesoporous TS-1, CMK-3, Carbon black, Oxidative desulfurization

### Introduction

Sulfur removal in transportation fuels is necessary in order to reduce the pollution level in the atmosphere, and currently ultra-deep desulfurization of fuel oil is receiving a worldwide attention ever since the announcement of the stringent U. S. environmental regulations imposed, limiting the sulfur level in diesel to < 15 ppmw.\(^6\)\(^7\) The most common industrial process for desulfurization is the treatment of the fuel with hydrogen at high temperature and high pressure conditions.\(^6\) Whilst this conventional hydrodesulfurization (HDS) is highly efficient at high temperature lower than 80 °C, it is being considered as one of the most promising options for the ultra-deep desulfurization.\(^6\)\(^7\)

For ODS, Ti-containing zeolites have been extensively investigated as catalyst because of their outstanding oxidation property and utilization of peroxides having an environmentally-benign nature as oxidant.\(^8\)-\(^10\) It is known that some small sulfides such as mercaptan, thiocarbonyl, and thiophene, a highly stable organic sulfide, can be effectively oxidized by TS-1 catalyst.\(^11\) However, conventional microporous TS-1 shows poor catalytic activity in the oxidation of bulkier sulfur compounds such as dibenzothiophene (DBT) and its derivatives, due to intracrystalline diffusion limitations imposed by small pores. Therefore, efforts have been made to resolve this diffusion limitation problem in TS-1 by introducing mesopores, and several template synthesis techniques that enable a preparation of zeolites having mesopores have newly emerged. In particular, much attention has been given to the synthesis of mesopore-containing zeolites via nanocasting by employing various sacrificial carbon templates in the hydrothermal synthesis of zeolites.\(^12\)-\(^17\)

In this work, we conducted a systematic comparison of the synthesis routes for making mesoporous TS-1, and detailed characterization of the mesoporous TS-1 zeolites prepared by employing two different carbon templates (carbon black and CMK-3) was reported. We carried out a probe reaction of allylchloride epoxidation using \( \text{H}_2\text{O}_2 \) as oxidant to confirm the nature of catalytic Ti sites in all the TS-1 samples prepared. Finally, it was demonstrated that the mesoporous TS-1 samples exhibit superior catalytic performances in oxidative desulfurization of selected bulky sulfur compounds to conventional TS-1, which were also influenced by the property of the carbon template used.

### Experimental

#### Synthesis of mesoporous TS-1.

For the synthesis of mesoporous TS-1, CMK-3 and carbon black (N762, Degussa) were used as solid template. SBA-15 was prepared following the literature procedure reported earlier,\(^18\) and the calcined SBA-15 was then used as template for making CMK-3. CMK-3 was prepared according to the literature procedure.\(^19\) The CMK-3 produced had the BET area of 1070 m\(^2\)g\(^{-1}\) and the total pore volume of 1.1 cm\(^3\)g\(^{-1}\). N762 has, on the other hand, had the BET area of 124 m\(^2\)g\(^{-1}\) and the total pore volume of 0.22 cm\(^3\)g\(^{-1}\). The carbon black consists of nearly spherical primary particles with typical diameters ranging from 20 to 150 nm.

Mesoporous TS-1 was prepared following the dry gel synthesis procedure reported by Jacobsen et al.\(^6\) CMK-3 (1.0 g) or carbon black (4.0 g) was impregnated with a clear solution containing tetrapropylammonium hydroxide (TPAOH, 40 wt%, TCI, 3.3 g) and ethanol (3.3 g). After evaporating ethanol at 40 °C, a mixture of tetraethylorthosilicate (TEOS, 98 wt%, Aldrich) and tetrabutylorthotitanate (TBOT, 97 wt%, Aldrich) was added with incipient wetness. The molar composition of the resulting synthesis gel was kept to 20 TPA\(_2\):TiO\(_2\):100 SiO\(_2\):200 H\(_2\)O. The gel was transferred into a Teflon liner containing sufficient water to produce saturated steam. The liner was placed inside a stainless steel autoclave and heated at 170 °C.
for 72 h. After the hydrothermal reaction, the autoclave was quenched in cold water and the powder was recovered by filtration and washed with de-ionized water. The final powder was calcined in air at 550 °C for 8 h to remove the organic structure-directing agent. For comparison, a conventional mesoporous TS-1 with similar titanium content synthesized according to Ref. 20.

**Characterization.** The crystallinity of the samples prepared was measured by X-ray diffraction using CuKα radiation (Phillips, PW-1700). Nitrogen adsorption-desorption isotherms were measured using a Micromeritics ASAP-2020 instrument at 77 K. UV-Visible spectra were obtained under ambient conditions using dehydrated MgO as a reference in the range of 190 - 500 nm on a Varian CARY-3E double beam spectrometer. Scanning electron microscopy (SEM) was performed using Hitachi S-4300 electron microscope, and transmission electron microscopy (TEM) measurements were taken on a Philips CM200.

**Catalytic study.** Allylchloride epoxidation using H₂O₂ (30 wt%, Aldrich) as oxidant was performed using Chemistation PPS-2510 fitted with a condenser (Eyela). The reaction was carried out at 318 K for 2 h using 32 mmol substrate, 17 mmol H₂O₂, 20 mL methanol, and 0.15 g catalyst under vigorous stirring. The products were analyzed by using a gas chromatography (HP5890 series II GC). The concentration of H₂O₂ after a reaction was determined by 0.1 M cerium sulfate titration using ferroin indicator.

The ODS reactivity of model sulfur compounds was studied in a 100 mL glass batch reactor equipped with a temperature controller, a condenser, and a mechanical stirrer. Typically, 48 g of feed (n-heptane 80 wt% and toluene 20 wt%) containing model sulfur compounds of 200 ppmw-S with a molar ratio of tert-butyl hydroperoxide (TBHP)/S of 2.5 was heated at 80 °C and stirred at 400 rpm followed by addition of 0.12 g of catalyst. The reaction products were analyzed by gas chromatography (Young Lin ACME 6000 GC, Korea) equipped with a PFPD (Pulsed Flame Photometric) detector.

**Results and Discussion**

X-ray powder diffraction patterns of the calcined TS-1 samples prepared are shown in Fig. 1. All the TS-1 samples were highly crystalline, showing the identical characteristic peaks corresponding to the zeolite MFI structure.

The UV-Vis spectra of the samples (Ti/Si = 0.01) are shown in Fig. 2. The spectra of the conventional TS-1 sample (c) show an absorption band around 210 nm, which corresponds to tetrahedral Ti(IV) coordination species in the framework. The absence of a shoulder at 260 - 270 nm corresponding to oligomeric Ti species and 330 - 350 nm peak corresponding to anatase phase in the UV-Vis spectra suggests that the sample is essentially free from extra-framework Ti species. The TS-1 samples prepared using carbon templates (a) and (b), on the other hand, exhibited a trace of oligomeric Ti species near 260 nm. The UV-Vis spectral quality for the TS-1 samples prepared with carbon templates deteriorated further with an increasingly visible shoulder at 260 nm when the samples were prepared with the higher amount of titanium in Ti/Si mol ratio of 2 (not shown). It seems the presence of the heterogeneous carbon...
Table 1. Textural properties of the TS-1 samples prepared

<table>
<thead>
<tr>
<th>Sample</th>
<th>Template source</th>
<th>(V_{\text{micro}}) (cm(^3)/g)(^a)</th>
<th>(V_{\text{meso}}) (cm(^3)/g)</th>
<th>(D_{\text{meso}}) (nm)</th>
<th>(S_{\text{ext}}) (m(^2)/g)(^b)</th>
<th>(S_{\text{BET}}) (m(^2)/g)(^c)</th>
</tr>
</thead>
<tbody>
<tr>
<td>meso-TS-1</td>
<td>CMK-3</td>
<td>0.12</td>
<td>0.31</td>
<td>14.7</td>
<td>110</td>
<td>388</td>
</tr>
<tr>
<td>meso-TS-1</td>
<td>Carbon black</td>
<td>0.15</td>
<td>0.14</td>
<td>6.8</td>
<td>106</td>
<td>440</td>
</tr>
<tr>
<td>conv-TS-1</td>
<td>-</td>
<td>0.16</td>
<td>0.07</td>
<td>-</td>
<td>121</td>
<td>428</td>
</tr>
</tbody>
</table>

\(^a\)Calculated by the \(t\)-plot method. \(^b\)Calculated by the BJH method (desorption). \(^c\)Calculated by the BET method.

phase in the substrate mixture inhibits the uniform mixing of titanium and silicon alkoxide precursors during the synthesis of TS-1.

Fig. 3 shows the nitrogen adsorption-desorption isotherms of the TS-1 samples after removing the carbon templates by calcination. The isotherms of TS-1 synthesized with CMK-3 (a) and carbon black (b) exhibited a hysteresis loop at relative pressures higher than \(P/P_0 = 0.4\), clearly indicating the existence of mesopores.\(^d\) The BET surface areas, \(t\)-plot external surface areas, pore volumes and the BJH average mesoporous sizes are given in Table 1. Whilst the micropore volumes estimated by the \(t\)-plot method for the three TS-1 samples are reasonably close to one another, TS-1 synthesized with CMK-3 has the largest mesopore volume (0.31 cm\(^3\)/g) over the conventional TS-1 (0.07 cm\(^3\)/g) and has a significantly large average pore size. TS-1 synthesized with carbon black also has shown a mesopore volume (0.14 cm\(^3\)/g) accompanied by the average pore size in the mesopore range associated with textural mesoporosity. The pore size distribution curves of the TS-1 catalysts prepared were shown in the inset of Fig. 3. The TS-1 synthesized with CMK-3 shows a narrow peak centered at 3.7 nm and broad range of pores distributed between 10 to 80 nm. On the other hand, the TS-1 synthesized with carbon black exhibited a bimodal pore size distribution; one in the range of 1.8 to 3 nm and the other 40 to 60 nm. As expected, the conventional TS-1 shows negligible mesopore volume. This analysis of pore size distribution shows that mesopores are successfully created by removing the carbon templates by calcination, but a small portion of macropores were also detected.

Fig. 4 shows the scanning electron microscopy (SEM) images of TS-1 samples after removal of the carbon templates. All TS-1 samples appear to be highly crystalline with no amorphous phases detected on their external surfaces. The crystal sizes of TS-1 catalysts as determined from SEM were \(ca. 0.2 - 0.3 \mu m\) for mesoporous TS-1 with CMK-3, 0.2 - 1.2 \(\mu m\) for mesoporous TS-1 with carbon black, and 0.3 - 0.4 \(\mu m\) for conventional TS-1, respectively. It is surprising that we could have TS-1 with smaller particle size than the conventional sample using CMK-3 templates, which will prove beneficial in liquid phase catalytic reactions involving large organic molecules due to their shorter diffusion path. We are speculating that the CMK-3 particles could have acted as a seed for TS-1 nucleation. TS-1 with carbon black, on the other hand, produced a bimodal distribution of particle size, which may be a consequence of the relatively wide particle size distribution in the carbon black, N762 (Degussa) as mentioned earlier.

Transmission electron microscopy (TEM) was attempted to visualize the actual nanoporous structure of the TS-1 samples prepared, and Fig. 5 shows the corresponding TEM images. Whilst it was difficult to make a clear observation of the mesopores created by carbon template as was reported by others,\(^{16,17}\) we could locate several grey spots of irregular mesopores in the TS-1 samples synthesized with carbon templates in (a) and (b), which were absent in the conventional TS-1 sample shown in (c).

Epoxidation of allylchloride (ALC) was chosen as a probe reaction to compare the catalytic properties of the TS-1 samples prepared; ALC is a sufficiently small organic molecule that can be accommodated inside the 10-membered ring pores of the conventional microporous TS-1. As shown in Table 2, conventional TS-1 showed the highest ALC conversion (21.7%) and mesoporous TS-1 catalysts exhibited a little lower catalytic activities than conventional TS-1; TS-1 prepared with CMK-3 (18.7% ALC conversion) was somewhat better in catalytic performance than the TS-1 prepared with carbon black (17.5%). We believe the differences in catalytic activities are caused by the minor differences in Ti states mentioned in Fig. 2.

![Figure 4. SEM images of (a) TS-1 synthesized with CMK-3, (b) TS-1 synthesized with carbon black, and (c) conventional TS-1.](image-url)
earlier, since it is known that tetrahedral Ti sites being more catalytically active than the oligomeric ones in TS-1. All TS-1 catalysts showed satisfactory H$_2$O$_2$ selectivities; 98.3% for TS-1 synthesized with CMK-3, 95.0% for TS-1 synthesized with carbon black, and 99.9% for conventional TS-1. Product selectivity to epichlorohydrin (ECH) was close to 100% with only trace amounts of side products such as dichlorohydrin or 3-chloro-1,2-propanediol detected.

Finally, oxidative desulfurization of DBT and 4,6-DMDBT with tert-butyl hydroperoxide as oxidizing agent over the TS-1 catalysts were conducted and the results are shown in Fig. 6 and Fig. 7, respectively. As shown in the figures, substantial enhancement in catalytic activity was achieved in mesoporous TS-1 catalysts compared with conventional TS-1. More specifically, catalytic ODS activities of the catalysts varied in the following order: conventional TS-1 $<$ mesoporous TS-1 with carbon black $<$ mesoporous TS-1 with CMK-3 for both DBT and 4,6-DMDBT. These results can be understood when we realize that the molecular dimensions of DBT (8.0 $\times$ 12.2 Å$^2$) and 4,6-DMDBT (8.7 $\times$ 12.2 Å$^2$) are significantly larger than the pores of conventional TS-1 zeolite (5.6 $\times$ 5.3 Å). Therefore, it is reasonable to assume that molecules like DBT and 4,6-DMDBT cannot have an access to the redox-active sites located inside the pores of conventional TS-1, and the improved catalytic activities of the mesoporous TS-1 catalysts must be attributed to their improved diffusion properties compared with conventional TS-1. In addition, mesoporous TS-1 prepared using CMK-3 produced better catalytic performances than the one prepared using carbon black, since the former has the larger mesopore volumes as well as the larger average pore diameters in TS-1. In addition, smaller particle size of the

### Table 2. Catalytic activities of the TS-1 samples prepared in allylchloride epoxidation using H$_2$O$_2$.

<table>
<thead>
<tr>
<th>Sample</th>
<th>Template source</th>
<th>Conversion (CL)</th>
<th>Selectivity (%)</th>
<th>Conversion (ECH)</th>
<th>Selectivity (%)</th>
<th>H$_2$O$_2$ Conversion (%)</th>
<th>H$_2$O$_2$ Selectivity (%)</th>
</tr>
</thead>
<tbody>
<tr>
<td>meso-TS-1 CMK-3</td>
<td>ALC + ECH + H$_2$O$_2$</td>
<td>18.7</td>
<td>$&gt;$ 99%</td>
<td>35.8</td>
<td>98.3</td>
<td></td>
<td></td>
</tr>
<tr>
<td>meso-TS-1 Carbon black</td>
<td>ALC + ECH + H$_2$O$_2$</td>
<td>17.5</td>
<td>$&gt;$ 99%</td>
<td>34.7</td>
<td>95.0</td>
<td></td>
<td></td>
</tr>
<tr>
<td>conv-TS-1</td>
<td>-</td>
<td>21.7</td>
<td>$&gt;$ 99%</td>
<td>41.2</td>
<td>99.9</td>
<td></td>
<td></td>
</tr>
</tbody>
</table>

![Figure 5](image-url) TEM images of (a) TS-1 synthesized with CMK-3, (b) TS-1 synthesized with carbon black, and (c) conventional TS-1 (The circles in figures (a) and (b) indicate the regions of meso-macro pores).

![Figure 6](image-url) Catalytic oxidation of DBT using TBHP as an oxidant by (a) TS-1 synthesized with CMK-3, (b) TS-1 synthesized with carbon black, and (c) conventional TS-1.

![Figure 7](image-url) Catalytic oxidation of 4,6-DMDBT using TBHP as an oxidant by (a) TS-1 synthesized with CMK-3, (b) TS-1 synthesized with carbon black, and (c) conventional TS-1.
TS-1 prepared with CMK-3 will also be useful for the reactions due to the shorter diffusion path of the reactants. As shown in Fig. 6 and Fig. 7, conventional TS-1 still produced significant conversions of 29.6% for DBT and 22.7% for 4,6-DMDBT after 3 h reaction. Apparently, ODS reaction can also take place at the catalyst external surfaces as well as inside the pores of TS-1 catalysts.

Conclusions

Mesoporous TS-1 catalysts were prepared using CMK-3 and carbon black as templates. The synthesized mesoporous TS-1 catalysts were found to exhibit substantially enhanced catalytic activities than a conventional microporous TS-1 catalyst in the oxidative desulfurization (ODS) of bulky sulfur compounds by providing easy access of the reactants to the active redox sites. CMK-3 was proven more effective to generate mesopores in TS-1 and also resulted in smaller particle size useful in liquid phase ODS reactions.

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References