Synthesis of thin-multiwalled carbon nanotubes by Fe-Mo/MgO catalyst using sol-gel method

Prashant Dubey¹, Sang Kyu Choi², Bawl Kim² and Cheol Jin Lee²,*

¹Centre of Material Sciences, Institute of Interdisciplinary Studies, University of Allahabad, Allahabad-211002, India
²School of Electrical Engineering, Korea University, Seoul 136-713, Korea

Received 7 January 2012
Accepted 13 February 2012
*Corresponding Author
E-mail: cjlee@korea.ac.kr
Tel: +82-2-3290-3216

Abstract
The sol-gel technique has been studied to fabricate a homogeneous Fe-Mo/MgO catalyst. Ambient effects (air, Ar, and H₂) on thermal decomposition of the citrate precursor have been systematically investigated to fabricate an Fe-Mo/MgO catalyst. Severe agglomeration of metal catalyst was observed under thermal decomposition of citrate precursor in air atmosphere. Ar/H₂ atmosphere effectively restricted agglomeration of bimetallic catalyst and formation of highly-dispersed Fe-Mo/MgO catalyst with high specific surface-area due to the formation of Fe-Mo nanoclusters within MgO support. High-quality thin-multiwalled carbon nanotubes (t-MWCNTs) with uniform diameters were achieved on a large scale by catalytic decomposition of methane over Fe-Mo/MgO catalyst prepared under Ar-atmosphere. The produced t-MWCNTs had outer diameters in the range of 4-8 nm (average diameter ~6.6 nm) and wall numbers in the range of 4-7 graphenes. The as-synthesized t-MWCNTs showed product yields over 450% relative to the utilized Fe-Mo/MgO catalyst, and indicated a purity of about 85%.

Key words: thermal decomposition, citrate precursor, nanoclusters, thin-multiwalled carbon nanotubes

1. Introduction

Thin-multiwalled carbon nanotubes (t-MWCNTs), which have outer diameters of less than 10 nm and graphene layers of 3-7 numbers, can be considered as an interface between single-walled CNT (SWCNT) and MWCNT structures. Recent experimental results showed that the t-MWCNTs have good electrical and mechanical properties, and excellent electron field emission properties [1-3]. These characteristics make them one of the most promising candidates for bulk applications such as CNT-polymer composites, CNT film, and CNT field emission. There has been a recent flurry of interest by several researchers to synthesize t-MWCNTs by catalytic chemical vapor deposition (CCVD) [1,4-6]. In the previous catalyst fabrication methods for t-MWCNT synthesis, a combustion process has commonly been used to obtain Fe-Mo/MgO, [1,4] Ni-Mo/MgO [5] or Co-Mo/MgO [6] catalyst materials. To prepare a homogeneous and efficient catalyst, it is desirable to fabricate well dispersed catalyst nanoparticles without agglomeration on the support materials [7-9]. However, there are two major problems for catalyst fabrication using a conventional combustion process: (i) difficulty of the process and poor reproducibility for the fabrication of homogeneous catalyst material due to a very fast and violent combustion process [10], and (ii) severe agglomeration of catalyst nanoparticles during the sintering process at the time of CNT growth.

Several studies have been dedicated to the fabrication of catalyst materials in order to achieve homogeneous and efficient catalyst particles. Coquay et al. [11,12] attempted to obtain a well-dispersed Fe catalyst on an MgO support by urea-combustion. They observed a poorly dispersed metal oxide catalyst, which was responsible for the uncontrolled growth
of non-homogeneous CNTs. Flahaut et al. [13] reported the formation of (Mg, Co, Mo)O solid solutions, which showed large diameter MWCNTs (inner diameter ~9 nm) having up to 13 graphene walls due to the used of high Mo content. It has commonly been accepted that the addition of Mo within transition metals like Fe, Co, or Ni increases the carbon yield and induces large diameter MWCNTs with defective structures at the side walls [5,13-17]. The realization of highly homogeneous catalyst nanoparticles with uniform size using a simple and low cost process is still a hot issue. Thus, we have studied a way to solve these problems using the sol-gel method. Unlike the highly exothermic combustion process, the sol-gel method is easy and simple to control and suitable for scale-up to the kilogram level [18]. In general, the sol-gel process involves the evolution of inorganic networks through formation of a colloidal suspension (sol) and gelation of the sol to form a three dimensional network in a continuous liquid phase (gel). In a recent paper we reported the synthesis and field emission properties of high-quality t-MWCNTs over an Fe-Mo/MgO catalyst based on the sol-gel technique [19]. With the extension of our previous work, we report here details about the fabrication and characterization of well-dispersed and homogeneous Fe-Mo/MgO catalyst materials with effective doping of high Mo content based on a sol-gel precursor method for the synthesis of high-quality t-MWCNTs. The conceptual idea originates from the shielding effect of Mo, which protects against agglomerations of Fe nanoparticles by effectively forming Fe-Mo nanoclusters that are well-dispersed within the MgO catalyst support. The purpose of the present report is to investigate the influence of gaseous atmosphere during thermal decomposition of a citrate precursor to fabricate Fe-Mo/MgO catalyst for high-quality t-MWCNT growth.

2. Experimental section

2.1. Preparation and characterization of Fe-Mo/MgO catalysts

The catalysts were prepared by a citrate precursor based on the sol-gel technique using MgO as catalyst support. An Fe-Mo/MgO catalyst was prepared according to the following procedure: the desired amount of Fe(NO$_3$)$_3$·9H$_2$O (99.99%, Aldrich) and Mg(NO$_3$)$_2$·4H$_2$O (99.99%, Aldrich) were dissolved in 20 mL deionized (DI) water. Then, citric acid was added as a complexing agent at a ratio of metal ion to citric acid of 1:1.2, followed by the addition of (NH$_4$)$_2$MoO$_4$·4H$_2$O (Aldrich) as Mo source. After stirring the heterogeneous mixture at 90°C for 30-40 min, a very homogeneous solution was obtained. In our experimental conditions, a mole ratio of Fe:Mo:MgO = 1:1.5:10 was the best composition to obtain homogeneous t-MWCNTs. The homogeneous solution was slowly evaporated on a hot plate to form a viscous gel. Then, the gel was kept for drying at 120°C in an oven for 5 h to remove the adsorbed water. During this process, the gel swelled into a yellow colored fluffy mass (which we call in this paper the ‘citrate precursor’). The citrate precursor was then ground into a fine powder. Finally, the citrate precursor was thermally decomposed under air, Ar (500 sccm), and H$_2$ (500 sccm) atmosphere at 700°C for 2 h in a quartz tube furnace to obtain Fe-Mo/MgO catalyst materials for CNT growth.

Powder X-ray diffraction (XRD, Rigaku D/MAX Rint 2000, diffractometer) analysis of the catalyst materials was carried out at room temperature using Cu Kα radiation (1.5418 Å) and a graphite secondary beam monochromator. The samples were mounted on a glass plate for X-ray measurements. Intensity was measured by a step scan in the 20 range of 10-80° with a step of 0.05° and by a measuring time of 5 s per point.

Nitrogen adsorption-desorption isotherms were measured at 77 K with an automatic vapor adsorption measurement system, BEL SorpMax, after outgassing at 10$^3$ Pa for 12 h at 120°C. These isotherms provided the Brunauer-Emmett-Teller (BET) specific surface area, pore volume, and pore size analysis of Fe-Mo/MgO catalyst materials.

The chemical state of the Fe-Mo catalysts after calculations was characterized using X-ray photoelectron spectroscopy (XPS, VG-scientific ESCALAB 250 spectrometer) equipped with Al-Kα radiation with a photon energy of 1486.6 eV. To decrease the influence of oxidation and the contamination of the XPS samples, these catalyst materials were sealed in a plastic box filled with Ar gas as soon as they were removed from the furnace; materials were then transferred to the analysis chamber (2.0 × 10$^{-9}$ torr) through a loading chamber (5.3 × 10$^{-9}$ torr) for XPS measurements.

2.2. Synthesis and characterization of CNTs

The synthesis of t-MWCNTs was carried out in a quartz tube reactor (10 cm i.d. and 120 cm length) mounted in a tube furnace. An amount of 0.1 g of calcined catalyst was placed into a quartz boat at the center of the reactor tube and heated to the reaction temperature (900°C) in an Ar (1000 sccm) atmosphere. Once the temperature reached 900°C, the catalyst was pretreated for 20 min in an Ar/H$_2$ (800/200 sccm) stream. Immediately after this pretreatment, the mixture of Ar/CH$_4$/H$_2$ (1000/1000/200 sccm) was supplied into the tube reactor at 900°C for 30 min in order to synthesize CNTs. Finally, the reactor was cooled to room temperature in an Ar (500 sccm) stream. These products are referred to hereafter as as-synthesized t-MWCNTs. The carbon weight-gain of each Fe-Mo/MgO catalyst has been calculated using the following Eq. (1):

$$C_{\text{weight-gain}}(\%) = \left[\frac{w_{\text{tot}} - w_{\text{cat}}}{w_{\text{cat}}}\right] \times 100$$

where $w_{\text{tot}}$ is the weight of the catalyst before the CNT growth and $w_{\text{cat}}$ is the total weight of the catalyst and carbon material after the CNT growth.

The morphologies and microstructures of the as-synthesized carbon materials over the Fe-Mo/MgO catalysts synthesized by thermal decomposition of citrate precursor under various atmospheres were initially characterized by scanning electron microscopy (SEM, Hitachi S-4700), operated at an accelerating voltage of 15 kV. Samples were deposited onto conductive carbon tape, which was attached to the surface of the SEM brass stub. These samples were then conductively coated with platinum by sputtering for 20 s to minimize charging effects under SEM imaging conditions.

Transmission electron microscopy (TEM, JEOL JEM-2100F) was used to analyze the quality and structural parameters, such as diameter and wall number, of the CNTs obtained over differ-
ent catalysts. Samples were prepared by drying a few droplets of
the as-synthesized carbon product from an ethanolic dispersion
onto a 300 mesh holey Cu grid coated with a lacey carbon film.
TEM and high resolution TEM (HRTEM) images were obtained
at accelerating voltages of 120 kV and 200 kV, respectively.

Thermogravimetric analysis (TGA) data were collected with
a TA Q50 instrument to determine the carbon content and purity
of the as-synthesized products. Approximately 5.0 mg of the
as-synthesized carbon product was placed in a platinum pan
and the experiment was performed in a flowing air environment
at 30 mL/min with a heating rate of 5ºC/min.

Raman spectra of the as-synthesized carbon products without
any purification were recorded using an excitation wavelength
of 514.5 nm on a Raman spectrometer from Horiba Jobin-Yvon,
HR-800, equipped with an Olympus confocal microscope. The
final spectrum presented was an average of 5 spectra recorded
in different regions over the entire range of the samples.

3. Results and Discussion

3.1. Citrate precursor (sol-gel) process

We adopted the sol-gel method to fabricate the Fe-Mo/
MgO catalyst for the synthesis of t-MWCNTs. The success of
the sol-gel method mainly depends on the quality of the pre-
cursor solution. In our catalyst fabrication, Mg(NO$_3$)$_2$·6H$_2$O,
Fe(NO$_3$)$_3$·9H$_2$O and citric acid were dissolved in DI water. The
pH of this solution was found to be about 1.0; the initial color of
the solution was orange-red. (NH$_4$)$_6$Mo$_7$O$_{24}$·4H$_2$O was added
to the orange-red solution. After stirring the heterogeneous mixture
at 90ºC for 30-40 min, there was a dissolution of the molyb-
denum complex. The reaction could presumably be a complex
formation between an aqueous solution of molybdic acid (MoO$_2$$^+$) and citric acid at that acidic pH. The complex formation between
MoO$_2$$^+$ and citrate is well-known in different pH ranges [20].
The reaction is shown in Eq. (2):

$$\text{MoO}_2^{2+} + \text{Citric acid} \rightarrow \text{Citratomolybdate complex}$$  \hspace{1cm} (2)

In terms of chemical composition, the citrate precursor is
obtained from the aqueous solution containing Mg$^{2+}$, Fe$^{3+}$, and
Mo$^{6+}$ metal salts and polyfunctional citric acid. The hydroxyl
and carboxylic functional groups in the citric acid (containing
1 hydroxyl and 3 carboxylate groups per molecule) react chemi-
cally with the metal ions to form a complex or a precursor. The
structure of the precursor and the composition (metal: ligand)
depend on the pH of the solution. But for our purposes
it is assumed that one mole of citric acid binds with one mole
of metal ions (1:1). The citrate precursor solution was further
heated with constant stirring at 90ºC to form a gel. The trans-
formation of the sol to a semi-solid type gel was visible at this
stage. The gel was kept at 120ºC in the oven for 5 h to obtain
a very homogeneous yellow colored fluffy solid. In our sol-gel
precursor method, it should be mentioned here that the function
of the complexing agent (citric acid) is threefold: (i) stabiliz-
ing the precursor solution through formation of metal hydrox-
decomplexes during the gel formation; (ii) preventing precipita-
tion of MoO$_2$$^+$ in the form of MoO$_3$ due to formation of stable cita-
tomolybdate complexes (Eq. 2) at acidic pH; and (iii) acting as a
foaming agent to produce a large volume of fluffy solid (citrate
precursor). The Fe-Mo/MgO catalyst was prepared by thermal
decomposition of a citrate precursor at 700ºC for 2 h under vari-
ous atmospheres to evaluate the structure and the homogeneity
of the produced nanotubes; these atmospheres were an oxidiz-
ing atmosphere such as ‘air’ (SG-1), an inert atmosphere such as
‘Ar’ (SG-2), and a reducing atmosphere such as ‘H$_2$’ (SG-3).

3.2. Characterization of Fe-Mo/MgO catalysts

Powder XRD and BET surface area analyses were carried
out for all three Fe-Mo/MgO catalyst materials synthesized by
thermal decomposition of the citrate precursor under different
atmospheres. Fig. 1 shows the combined XRD patterns of the
three sol-gel catalysts (SG-1, SG-2 and SG-3). The XRD pat-
tern clearly shows the five well-resolved characteristic peaks of
the MgO rock-salt lattice in all three samples [21]. We were not
able to detect any separate phase for FeO$_x$ or MoO$_x$ from SG-2
and SG-3 catalysts (Figs. 1b and c), which means that the Fe
and Mo species have good dispersion within the MgO matrix.
For an ideal FeO-MgO solid solution, all iron should be in the
divalent state and should substitute for Mg$^{2+}$ [11]. As the ionic
radius of Fe$^{2+}$ is larger than the ionic radius of Mg$^{2+}$, FeO-MgO

\[ \text{thin-multiwalled CNTs by Fe-Mo/MgO catalyst} \]
solid solution is unfavorable for the high dispersion of Fe species compared to CoO-MgO or Ni-MgO solid solutions [22]. Here, we propose that Fe forms a stable cluster with Mo, and it exists predominantly in the Fe\(^{2+}\) state. Principally, these Fe-Mo clusters are anionic in nature and can strongly interact within the Mg\(^{2+}\) lattice to favor well-dispersed nanoparticles in the form of Fe-Mo/MgO. This hypothesis will be supported in the later section by TEM-energy dispersive X-ray spectrometer (EDS) and XPS studies. The XRD pattern of the SG-1 catalyst clearly showed different Mo phases such as MgMoO\(_7\), MgMoO\(_3\), and MoO\(_2\) (Fig. 1a) which are invisible in the SG-2 and SG-3 catalysts [17,23]. In the case of the SG-3 catalyst, we observed the Mo\(_2\)C phase from XRD (Fig. 1c); this phase may be attributed to the reducing H\(_2\) atmosphere and the carbon supply from the burning of the citric acid at 700ºC [24]. Thus, from XRD analysis, it is understood that Fe-Mo/MgO catalysts produced by thermal decomposition of the citrate precursor under Ar and H\(_2\) atmospheres are well-mixed bimetallic catalysts compared to those catalysts produced in an air atmosphere.

Fig. 2 shows the nitrogen adsorption and desorption isotherms of the three Fe-Mo/MgO catalyst materials synthesized by thermal decomposition of citrate precursor at 700ºC for 2 h.

![Fig. 2. Nitrogen adsorption and desorption isotherms of Fe-Mo/MgO catalyst materials synthesized by thermal decomposition of citrate precursor at 700ºC for 2 h.](image)

### Table 1. Pore diameter, pore volume and BET surface area of Fe-Mo/MgO catalyst materials and carbon yields obtained on these catalysts based on weight gain measurements (Eq. 1) and TGA analysis (value given within small bracket indicates MgO support material without Fe and Mo content)

<table>
<thead>
<tr>
<th>Catalyst materials</th>
<th>Pore diameter (nm)</th>
<th>Pore volume (cm(^3)/g)</th>
<th>Surface area (m(^2)/g)</th>
<th>Product yield (%)</th>
<th>Carbon % yield @TGA</th>
</tr>
</thead>
<tbody>
<tr>
<td>SG-1</td>
<td>11.4 (9.2)</td>
<td>0.17 (0.13)</td>
<td>60 (55)</td>
<td>73</td>
<td>43</td>
</tr>
<tr>
<td>SG-2</td>
<td>2.8 (3.3)</td>
<td>0.14 (0.22)</td>
<td>202 (261)</td>
<td>452</td>
<td>85</td>
</tr>
<tr>
<td>SG-3</td>
<td>2.8 (3.3)</td>
<td>0.15 (0.20)</td>
<td>210 (253)</td>
<td>370</td>
<td>82</td>
</tr>
</tbody>
</table>


The isotherm therefore indicates that both SG-2 and SG-3 catalysts possess good structural ordering and a narrow pore size distribution compared to those of the SG-1 catalyst. The difference observed in the adsorption isotherm of the Fe-Mo/MgO catalysts is attributed to the difference in the preparation conditions. The Ar or H\(_2\) atmosphere induces uniform sized Fe-Mo bimetallic catalysts with homogeneous distribution within MgO pores; air atmosphere, on the other hand, leads to a non-uniform Fe-Mo catalyst.

The BET surface area, pore diameter and pore volume of Fe-Mo/MgO catalysts are also found to depend on the decomposition atmosphere of the citrate precursor. The results are summarized in Table 1. It can be observed that the BET surface area of the SG-1 catalyst material is very low compared to that of the SG-2 or SG-3 catalysts. The surface areas observed for the SG-2 or SG-3 catalyst materials are comparable. Furthermore, air decomposition of the citrate precursor leads to a large pore diameter and pore volume for the Fe-Mo/MgO catalyst. We also examined the surface properties of a material with only MgO support synthesized in the same conditions except for the addition of Fe and Mo species; this test is shown in the small brackets in Table 1. In an air atmosphere, we observed an increment of pore diameter and pore volume in the Fe-Mo/MgO catalyst (SG-1) compared with the material with only MgO support; however, the surface areas are comparable. This may be attributed to the non-uniform distribution of bimetallic nanoclusters and to phase separation of the catalyst materials due to the formation of Mg-O-Mg\(_2\)O\(_7\)/MgMoO\(_3\); these results further correlate with our XRD results, which were discussed in the previous section. However, Ar and H\(_2\) decomposed Fe-Mo/MgO catalysts (SG-2 and SG-3) showed decreased pore diameter, pore volume, and surface area compared to the case of the MgO support material. This behavior can be explained as being due to pore filling and the blocking phenomenon of metal precursors [26]; this behavior supports our hypothesis that Fe-Mo systems form in a well-dispersed manner within MgO support. The product yields of carbon materials were found to be correlated with the BET surface area of the starting Fe-Mo/MgO catalysts. It is generally understood that a large surface area with a small pore size of catalyst material may provide large numbers of active metal catalysts; this is the characteristic that is responsible for the high-yield carbon materials (Table 1). In the case of the SG-1 catalyst, the produced carbon material consisted of thick CNTs and carbon fibers, along with some t-MWCNTs and carbon fibers, along with some t-MWCNTs and carbon fibers, along with some t-MWCNTs and carbon fibers, along with some t-MWCNTs and carbon fibers, along with some t-MWCNTs and carbon fibers.
MgO catalyst materials prepared by thermal decomposition of the citrate precursor under different atmospheres. In the case of the SG-1 catalyst, we can observe a non-uniform distribution of catalyst particles (dark spots) on the MgO support material, as shown in Fig. 3a. The TEM observation is consistent with the surface analysis results, in which the SG-1 catalyst shows a low BET surface area and a large pore diameter. On the other hand, we can observe well-dispersed nanosized particles as dark spots in the case of the Ar (SG-2) and H\textsubscript{2} (SG-3) atmospheres, as shown in Figs. 3b and c. The size of the dark spots was measured and found to be in the range of 3-6 nm for the SG-2 and SG-3 catalysts (inset of Figs. 3b and c). We further analyzed the TEM-EDS of the dark spots at a 1.0 nm target point, which showed a higher atomic % of Mo compared with that of Fe in the cases of SG-2 (at% Fe:Mo \sim 3.1:10.5) and SG-3 (at% Fe:Mo \sim 3.0:12.1) catalysts, while the atomic % of Fe is higher in the case of the SG-1 (at% Fe:Mo \sim 7.9:4.2) catalyst. Therefore, we conclude that in the case of Ar and H\textsubscript{2} decomposition atmospheres, the formation of Fe-Mo nanosized clusters with higher Mo content is predominant and Mo protects against the agglomeration of Fe nanoparticles. However, in the case of an air decomposition atmosphere, Fe appears to be more actively agglomerated because of the phase separation between Fe and Mo particles and because Mo doesn’t react with Fe during the formation of nanoparticles. This result is also supported by XRD, which show well-mixed Fe-Mo/MgO bimetallic catalyst in the case of SG-2 and SG-3 catalysts, while SG-1 showed various Mo phases with strong interaction among Mg ions.

Fig. 4 shows the Mo 3d core level XPS spectra of the citrate precursor and the Fe-Mo/MgO catalyst materials synthesized after thermal decomposition in various atmospheres. In the case of the citrate precursor (Fig. 4a), the XPS exhibits a pair of spin-orbit binding energies (BEs) at 231.0 and 234.0 eV. The Mo 3d\textsubscript{5/2} BE at 231.0 eV is attributed to Mo\textsuperscript{6+} in the citratomolybdate complex; this value is slightly lower than that of Mo\textsuperscript{6+} in MoO\textsubscript{3} (232.2-233.0 eV) due to the complex formation, whereas the second BE at 234.0 eV can be assigned to the Mo 3d\textsubscript{3/2} of the citratomolybdate complex. After thermal decomposition in air (Fig. 4b), a pair of spin-orbit BEs shifted towards higher values at 232.2 and 235.4 eV; these values are assigned to Mo\textsuperscript{6+} in MoO\textsubscript{3} or to MgMo\textsubscript{x}O\textsubscript{y} [27]. It can be observed that the XPS of the SG-2 and SG-3 catalysts exhibit a pair of spin-orbit BEs at 231.1 and 234.3-234.4 eV, whereas a new component appeared at 228.3-229.1 eV (Figs. 4c and d). The Mo (3d\textsubscript{5/2} and 3d\textsubscript{3/2}) BEs at 231.1 and 234.3-234.4 eV can be assigned to the Mo\textsuperscript{6+} in nanoclusters [28-31]. Interestingly, Mo\textsuperscript{6+} BEs in the Mo 3d core level of SG-2 and SG-3 showed values that were slightly lower than those of the SG-1 catalyst (Fig. 4), which may be explained as in the case of the Ar and H\textsubscript{2} decomposition of the citrate precursor, in which Mo has a strong interaction with Fe. From a chemical point of view, Fe\textsuperscript{3+} and Mo\textsuperscript{6+} have strong tendencies to aggregate in the form of a cluster under a reducing atmosphere [32,33]. We consider that Mo provides a shielding effect for the Fe nanoparticles in the form of a nanocluster/allyl to prevent agglomeration at higher growth temperatures. The new Mo 3d\textsubscript{5/2} peak at lower BE for SG-2 and SG-3, at around 228.3-229.1 eV, is assigned to Mo\textsuperscript{6+}/Mo\textsuperscript{4+} in the nanocluster. So, these results indicate that the decomposition of the citrate precursor in air resulted in the
at 707.8-708.4 and 721.4-722.3 eV, which can be attributed to Fe$^{3+}$ (as Fe$_{2p}^{3/2}$ and Fe$_{2p}^{1/2}$) in nanoclusters [35,36].

3.3. Characterization of CNTs

Low and high-magnification SEM images of the as-synthesized carbon materials fabricated by catalytic decomposition of CH$_4$ over Fe-Mo/MgO catalysts: (a, b) SG-1, (c, d) SG-2 and (e, f) SG-3.

XPS of the Fe 2p core level for the citrate precursor as well as for the Fe-Mo/MgO catalyst materials synthesized by thermal decomposition at 700ºC for 2 h: (b) SG-1, (c) SG-2 and (d) SG-3 catalyst.

formation of Mo$^{6+}$ in MoO$_3$ and/or MgMoO$_x$, while the decomposition in Ar and H$_2$ atmosphere produced Mo$^{4+}$ and Mo$^{5+}$/Mo$^{6+}$ in the form of nanoclusters. Another important point to note is the linewidth of the XPS spectra (Fig. 4). The linewidths of the Mo 3d peaks obtained for the SG-2 and SG-3 catalysts were sharper than that for SG-1. A similar linewidth sharpening phenomenon has been observed for the Co-Mo catalyst system when Na is doped into the catalyst; the phenomenon is attributed to the formation of sodium molybdate [34]. Here in our experimental conditions, we assigned this to the strong interaction of Mo with Fe and the formation of clusters. Even though this observation cannot be perfectly conclusive, it agrees with the results obtained by XRD and EDS-TEM, which indicate a well-dispersed Fe-Mo bimetallic catalyst within the MgO matrix and the existence of a higher Mo/Fe atomic ratio within the 1.0 nm spot range.

XPS of the Fe 2p core level for the citrate precursor as well as for the Fe-Mo/MgO catalyst materials synthesized by thermal decomposition in various atmospheres are shown in Fig. 5. In the case of the citrate precursor (Fig. 5a), again a pair of spin-orbit BEs at 707.2 and 721.3 eV exhibit very low intensity; their peak intensity increased and shifted towards a higher value at 710.2 and 723.0 eV after thermal decomposition in air (Fig. 5b). In the case of the SG-1, both peaks are assigned to Fe$^{3+}$ (as Fe$_{2p}^{3/2}$ and Fe$_{2p}^{1/2}$) in Fe$_2$O$_3$ and/or FeMoO$_x$ [27]. Again, SG-2 (Fig. 5c) and SG-3 (Fig. 5d) showed a pair of spin-orbit BEs at 707.8-708.4 and 721.4-722.3 eV, which can be attributed to Fe$^{3+}$ (as Fe$_{2p}^{3/2}$ and Fe$_{2p}^{1/2}$) in nanoclusters [35,36].

In the case of the Ar and H$_2$ decomposition, again we observed one peak at a lower BE of around 701.5 eV; this peak is assigned to Fe$^{2+}$ or even to metallic Fe species in nanoclusters.

3.3. Characterization of CNTs

Low and high-magnification SEM images of the as-synthesized carbon products over SG-1, SG-2, and SG-3 catalysts are shown in Fig. 6. It can be observed that the Fe-Mo/MgO catalyst materials synthesized under various thermal decomposition atmospheres strongly influence the CNT growth in terms of CNT morphology and homogeneity. In the case of the SG-1 catalyst, we can observe thick CNTs and fiber-like structures along with narrow CNTs (Figs. 6a and b). The formation of carbon nanofiber may be due to the existence of large Fe particles on the catalyst. Mo has a small tendency to mix with Fe in the form of nanoclusters [12]. On the other hand, SG-2 and SG-3 catalysts produced abundant CNT products by catalytic decomposition of CH$_4$. The entangled CNTs fully covered the entire catalyst surface and we were hardly able to observe any MgO support materials (Figs. 6c and d). High-magnification SEM images (Figs. 6d and f) show that the as-synthesized CNTs have uniform diameters and clean surfaces without amorphous carbon impurities. It is noteworthy to mention that no purification was conducted before imaging. Thus, SEM observations qualitatively indicate that the produced CNTs have high yield, high homogeneity, and high purity in the cases of the SG-2 and SG-3 catalysts. To quantify the product yield of the CNTs, a weight gain measurement (Eq. 1) was done for the as-synthesized carbon materials. High
Thin-multiwalled CNTs by Fe-Mo/ MgO catalyst

Catalyst particles to prevent their agglomeration and to promote the aromatization of CH\textsubscript{4} at elevated temperature. It is well-known that the supported Mo compounds on zeolite, as well as a transition alumina, convert CH\textsubscript{4} into aromatic species [37-39]. For an Fe-Mo/MgO catalyst with a CH\textsubscript{4} carbon source at 900°C, it is plausible that intermediate aromatic hydrocarbons are generated at the Mo sites [40].

Fig. 7 shows TEM images of the as-synthesized carbon materials fabricated by catalytic decomposition of CH\textsubscript{4} over various Fe-Mo/MgO catalysts. The carbon material synthesized over the SG-1 catalyst shows a non-uniform CNT structure, which is also confirmed by SEM observations. One can clearly see that a mixture of t-MWCNTs, MWCNTs, and carbon fibers exists in the carbon products using the SG-1 catalyst (Fig. 7a). A representative HRTEM of the SG-1 derived t-MWCNTs is shown in Fig. 7b. On the other hand, a low-magnification TEM image clearly reveals the high-quality t-MWCNTs with uniform diameters synthesized by the SG-2 catalyst (Fig. 7c). Furthermore, SG-3 synthesized t-MWCNTs show homogeneity and other characteristics that are almost identical to those of SG-2 synthesized t-MWCNTs (Figs. 7c and e). In addition, it is very difficult to determine bundle morphology for the t-MWCNTs produced by the SG-2 catalyst; this is different from the case in previous reports, and indicates the mixture of isolated tubes and bundles of tubes [1,4]. This may be attributed to the formation of slightly larger diameter t-MWCNTs on the catalyst particles, which introduce a weak van der Waals interaction between the tubes. An HRTEM image of the as-synthesized t-MWCNTs over the SG-2 catalyst clearly indicates the resolved graphene layers and slightly amorphous carbon deposits on the t-MWCNT surface (Fig. 7d). This indicates that the as-synthesized t-MWCNTs are of high-quality. Moreover, the HRTEM observations indicate that the produced high-quality t-MWCNTs have only a few graphene walls in the range of 4 to 7 numbers.

We further evaluated the distributions of the outer diameters and the graphene wall numbers of the t-MWCNTs synthesized by SG-2 and SG-3 catalysts. We measured more than 150 isolated t-MWCNTs with an accuracy of about ± 0.1-0.15 nm, based on HRTEM images like those in Figs. 7d and f. In the case of the SG-2 catalyst, the average outer diameter of t-MWCNTs was obtained relative to the weight of the utilized catalyst, revealing a significantly higher product yield of carbon materials (Table 1). In our catalyst composition study, the Fe: Mo ratio was found to be crucial to the achievement of homogeneous t-MWCNTs at high yield. We obtained the best results at a molar ratio of Fe: Mo = 1:1.5; it is considered that the good catalyst activity was caused by the effective doping of high Mo content into the catalyst materials. The higher Mo content can provide an effective shielding for Fe catalyst particles to prevent their agglomeration and to promote the aromatization of CH\textsubscript{4} at elevated temperature. It is well-known that the supported Mo compounds on zeolite, as well as a transition alumina, convert CH\textsubscript{4} into aromatic species [37-39]. For an Fe-Mo/MgO catalyst with a CH\textsubscript{4} carbon source at 900°C, it is plausible that intermediate aromatic hydrocarbons are generated at the Mo sites [40].

Fig. 7. Typical low-magnification transmission electron microscope (TEM) and high resolution TEM images of the as-synthesized carbon materials fabricated by catalytic decomposition of CH\textsubscript{4} over Fe-Mo/MgO catalysts: (a, b) SG-1, (c, d) SG-2 and (e, f) SG-3.

Fig. 8. Thermogravimetric analysis weight loss curve (a) and the corresponding derivative curve (b) of the as-synthesized thin-multiwalled carbon nanotubes fabricated by catalytic decomposition of CH\textsubscript{4} over Fe-Mo/MgO catalysts.
of the SG-2 catalyst, more than 95% of the t-MWCNTs have outer diameters in the range of 4-8 nm, with a Gaussian mean diameter of 6.6 ± 0.1 nm; they also have graphene walls with numbers of 4-7. However, in the case of the SG-3 catalyst, most of the t-MWCNTs have outer diameters in the range of 4-9 nm, with a Gaussian mean diameter of 7.7 ± 0.1 and graphene walls with number of 5-8. Thus, it is considered that the t-MWCNTs produced by both SG-2 and SG-3 catalysts have homogeneous morphology and structure on top of their uniform diameters. Compared with previous reports on the synthesis of t-MWCNTs, which showed final outer diameter distributions in the range of 3-6 nm using Fe-Mo/MgO combustion catalyst [4], the t-MWCNTs in our report had slightly larger outer diameters, in the range of 4-8 nm. In an earlier report, low Mo content within the bimetallic catalyst (Fe₅₀Mo₃₀Mgₓ₋₅₋ₓO as catalyst) was used; also, CNT growth was performed in a small-scale reactor under a high flow rate of H₂ as a carrier gas [4]. Here it is worth mentioning that we could never have obtained high-yield and homogeneous t-MWCNTs in our experimental conditions using a low Mo concentration catalyst in a large-scale reactor (reactor i.d. ~100 mm). Here we consider that the slightly large diameter of our t-MWCNTs is due to the higher Mo concentration [13]. We suggest that the high Mo concentration is beneficial for the efficient decomposition of CH₄ and is favorable for the growth of high-yield and homogeneous t-MWCNTs.

TGA analysis was used to determine the carbon content and purity of the as-synthesized carbon products. Fig. 8a shows a comparative TGA weight loss curve of the as-synthesized carbon materials synthesized over three sol-gel catalysts. It is considered that the weight loss up to 500°C can be assigned to the burning of amorphous carbon materials and further loss up to 700°C can be assigned to the oxidation of CNTs [41]. A slight weight gain in the case of the SG-1 catalyst at around 500°C is due to the oxidation of the catalytic metals; further weight loss can be assigned to the burning of CNTs. The results indicate that the weight loss percentages of t-MWCNTs due to SG-2 and SG-3 catalysts are around 85% and 82% from 500 to 650°C, respectively. Before reaching the burning temperature, we were not able to see any significant weight loss in the TGA curve (Fig. 8a), which indicates that the as-synthesized t-MWCNTs consist of homogeneous carbon species without amorphous carbon. Interestingly, the differential thermogravimetric (DTG) curve of the as-synthesized CNTs from the SG-1 catalyst showed broad and weak peaks compared to the narrow width peaks from the SG-2 and SG-3 catalysts (Fig. 8b). The broadening of the DTG peak is attributed to the non-homogeneous structure of the CNTs, as confirmed by SEM and TEM observations. The TGA indicates that the t-MWCNTs synthesized by the SG-2 and SG-3 catalysts show homogeneity and purity higher than those of CNTs fabricated with the SG-1 catalyst. Raman spectroscopy was used to further investigate the overall information of the as-synthesized CNTs. The Raman spectra of CNT materials synthesized by SG-1, SG-2, and SG-3 catalysts are shown in Fig. 9. In the Raman spectra, the G-band, which appears at approximately ~1593 cm⁻¹, is associated with sp² hybridized carbon bonding (the in-plane stretching mode for graphene sheets), while the D-band at approximately ~1350 cm⁻¹ reveals the defect level, impurities, or lattice disordering in the graphite sheets. The peak intensity ratio of the G and D-bands (I_G/I_D) is frequently used to understand the structure and quality of CNT samples [42,43]. In the case of the t-MWCNTs synthesized by the SG-2 and SG-3 catalysts, we can observe a high I_G/I_D ratio compared to that of the CNTs synthesized by the SG-1 catalyst, which indicates structural perfection and low defect levels. These results are in good agreement with our HRTEM observations.

4. Conclusions

We have demonstrated a new and simple fabrication method for Fe-Mo/MgO catalyst materials using a citrate precursor and based on the sol-gel technique; we achieve high-quality t-MWCNTs with uniform diameters by CCVD. A systematic investigation of the effect of the ambient type (air, Ar, and H₂) on the thermal decomposition of the citrate precursor in the fabrication of Fe-Mo/MgO catalysts and nanotube growth was carried out. The results suggest that, compared with an air atmosphere, Ar and H₂ atmospheres were beneficial to achieving homogeneous and highly-dispersed Fe-Mo/MgO catalyst materials. Furthermore, uniformly distributing a lot of catalyst particles over the support material and effectively doping a high Mo content were the key parameters in the synthesis of homogeneous and high-quality t-MWCNTs on a large scale. In terms of chemical composition, the higher Mo content for the Fe-Mo/MgO catalyst induced a higher product yield and uniformity of the synthesized t-MWCNTs. It is suggested that the higher Mo content effectively promotes aromatization of CH₄ and increases homogeneously dispersed catalytic Fe sites over the support material, which results in an effective shielding against agglomeration at reaction temperature. The carbon materials mostly consisted of individual t-MWCNTs that were nearly free of defects, and amorphous carbon deposits on the nanotube surfaces. The outer tube diameters and the graphene walls of the as-synthesized t-MWCNTs over the SG-2 catalyst were in the range of 4-8 nm (average dia. ~6.6 nm) and had graphene numbers in the range...
of 4-7. In this work, the as-synthesized t-MWCNTs showed a high product yield of over 450% relative to the utilized Fe-Mo/ MgO catalyst and a high purity of about 85%.

Acknowledgements

This work was supported by, and supported by the Korea Foundation for International Cooperation of Science and Technology (KICOS) through a grant provided by the MOST in K20601000002-07E10100-00220, and supported by the Korea Basic Science Institute (KBSI).

References


http://dx.doi.org/10.1021/ef0602372.


